

Geothermal Materials Selection – Old Lessons, New Directions

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- Geothermal Materials Selection

 Rules of Thumb and Their Basis (H₂S Corrosion)
- New Rules for New Plant and Processes
 - Engineered Systems, i.e. pH Adjustment
- Anticipated Extremes for Future Development
 CO₂ Rich, Acid Fluids
- Asset Integrity Management

– Risk Based Assessment and Industry Groups.



- Carbon steel can be used in 2-phase fluid, steam and water because protective films are formed when oxygen is absent:
 - Oxygen must be avoided, design for scales and pitting.
- 2. Stainless steels are susceptible to pitting corrosion and Chloride Stress Corrosion Cracking (Chloride SCC) and Sulfide Stress Cracking (SSC):
 - Suitable corrosion resistant alloys must be selected.
- Hydrogen readily diffuses into steels and high strength alloys suffer SSC or Hydrogen Induced Cracking (HIC/HE):
 - Low strength steels with low stress levels are preferred.



Carbon steels form protective films in low chloride near neutral pH fluids

Kawerau Main Steam Pipeline Form of Corrosion Products

Core of corroding Fe with layer of magnetite underlying an outer layer of iron sulfide - pyrrhotite



S map

Optical Image Fe map

Lichti, 2006



Carbon steels form protective films in low chloride near neutral pH fluids

T = 160 C, pH = 6, H_2S = 10-4 mol/kg, SiO₂ = 4 mg/kg



572 hours 244 hours

Carbon steel corrosion and corrosion products

Inman, 1994



Carbon steels form protective films in low chloride near neutral pH fluids



Oxygen Contamination Effects

QUEST INTEGRITY GROUP Process • Pipeline • Power

Carbon steels form protective films in low chloride near neutral pH fluids



Selection of Corrosion Resistant Alloys (CRAs)





20KI

0683



Damage Mechanisms for CRAs (in this case):

- Localised Corrosion (at weld toe)
- Weld Attack (variable metallurgy)
- Fatigue and Corrosion Fatigue (propagation)
- Chloride Stress Corrosion Cracking or Sulfide Stress Cracking (side branching)
- Crevice Corrosion
- Acid Attack
- Sticksion and Galling

Lichti, 2006



Heated U-Bend with Steam Condensate



Selection of Corrosion Resistant Alloys



CI SCC REQUIRED CONDITIONS

- + Aeration (oxygen)
- + Corrosive Species
- + Evapourative Concentration
- + Moisture or wetness
- + Tensile Stress (residual)
- + T > 60°C
- + Material Susceptibility





Alloy 2RK65 63 weeks at 100°C Drip solution of :

- geothermal steam condensate
- 30 mg/kg chloride added

CI SCC Cracks May Propagate by Corrosion Fatigue

Lichti et al 1995



Hydrogen readily diffuses into steels and high strength alloys suffer Sulfide Stress Cracking (SSC) or Hydrogen Induced Cracking (HIC/HE) ANSI/NACE MR0175/ISO 15156-1:2009(E), -2, -3

Standard Material Requirement for Sulfide Stress Corrosion Cracking Resistant Metallic Materials for Oilfield Equipment

- Sour Water and Sour Gas Systems Definitions.
 - Geothermal Systems Always Considered as "sour."
- Hardness and Cold Work Limits for Accepted Alloys.
 - Use as low a Strength as can be tolerated by the Design.
- Heat Treatment Processes Specified.
- Materials for Specific Facilities Identified.





Fabricated Vessel

- Meets hardness criteria of NACE Standard
- Thickness at limit for heat treatment (ASME).
- Welded with limited number of passes – high heat input.
- High Residual Stress.
- HE or SSC?



pH Adjust and Heavy Metal Scaling

- Elemental Arsenic and Antimony observed with some pH adjusted Brines.
 - Galvanic and erosion corrosion sometimes observed
 - Reasons for heavy metal scaling not known
- GNS Science Sponsored Laboratory Studies
 - Effect of temperature
 - Effect of pH
 - Effect of aeration / oxidising potential
 - Effect of heavy metal (arsenic vs antimony) and Area Ratios

Erosion Corrosion associated with heavy metal deposition

Amend and Yee, 2013



pH Adjust and Heavy Metal Scaling

- GNS Science Sponsored R&D on Galvanic Corrosion
 - Effect of temperature
 - Effect of pH
 - Effect of aeration / oxidising potential
 - Effect of heavy metal (arsenic vs antimony) and Area Ratios





- Chemistry changes in heat exchanger leading to elemental arsenic precipitation
 - Oxidation of steel and reduction of heavy metal
 - Galvanic corrosion contribution to the failure

Oxidation of Iron Reduction of Arsenic Fe \rightarrow Fe²⁺ + 2e⁻ AsO⁺ + 2H⁺ + 3e⁻ \rightarrow As(s) + H₂O



CO₂ Corrosion - Corrosion Product Stability





Model Chemistry with pCO2 = 6.9 bara



Model Chemistry with pH2S = 0.02 bara

Lichti, unpublished results



Factors leading to risk of CO₂ Corrosion:

- Partial pressure of CO_2 lower pH gives higher risk
- Temperature lower temperatures give higher risk
- Flow Velocity lower soluble iron in solution gives higher risk
- Inhibitors H₂S at a low level reduces the risk of CO₂ Corrosion



T < 120°C

Humphreys et al, 2015



In-situ synchrotron X-ray diffraction (XRD) on Properties of Protective Films

- Study of Controlling Parameters for CO2 Corrosion
 - Effect of Alloying, Inhibitors, Flow Velocity, H2S Concentration
- Extension of New Zealand MBIE project Qatar University, Callaghan Innovation, Quest Integrity, GNS Science, University of Auckland, plus industry interested parties



- Flux of iron is varied.
- High nucleation rate when S_{crit} is reached followed by growth when supersaturation is below S_{crit}.
- Resulting in small crystallites.

Unknown factors in the experiments – why the conditions resulted in the formation of Fe₂(OH)₂CO₃ is not yet fully understood. **Potentiostatic Experiment (Recent Results 2012)**

Mild steel, E = -500mV vs. Ag/AgCl 3M KCl (OCP = -725mV)



Fe₂(OH)₂CO₃ was detected in the formed scale for mild steel under potentiostatic control – this was not observed previously and resulted in significantly different scale morphology.

Ko et al, 2012

Acidic Environments have different film properties





S4, pH 3, 150° C, SO₄⁼ + HS⁻, 24 h Major Fe(1+x)S Mackinawite Minor: FeS Troilite

S4, pH 5, 150° C, SO₄⁼ + HS⁻, 12 h Major: FeS Troilite Minor: Fe(1+x)S Mackinawite

Field and Laboratory pH Adjustment





Risk Based Assessment - Concepts



- Risk Based Assessment / Aging Power Plants
 - Likelihood of Failure: Damage Mechanisms, Location of Damage, Rate of Damage Accumulation
 - Consequences of Failure: Health and Safety, Environmental, Cost of Repair and Unplanned Outage
- Risk = Likelihood * Consequences
- Risk Based Inspection: Maintenance Planning, Focused Turnaround Efforts, To Industry Codes, No Unplanned Outage – Living Documentation for Lessons Learned
- Integrity Operating Windows Management of Change, Validity Range for Risk Assessment



Typical Damage Mechanisms





Lichti et al, 2005



 Erosion at Elbows Lichti et al, 2003 Localised Pitting Corrosion

Passive Film Formation

Ramos et al, 2003

Damage Mechanisms to Look For





Following the format in API 571

Lichti et al, 2013



- To understand damage mechanisms and expected lifetimes of geothermal steam turbines and associated components
- To participate in joint research projects
- To share experiences and exchange information
- To share information on design upgrades
- To research, develop and optimise inspection and refurbishment / replacement strategies







- 1. Oxygen corrosion can be controlled
- 2. Corrosion Resistant Alloys can be selected
- 3. ANSI/NACE MR0175/ISO 15156-2&3:2009(E) must be applied
- 4. Process and materials changes should be approached with caution:
 - New material-environment combinations present new problems
 - Start with the basics and test to verify assertions
- 5. Learning from Experience and Sharing
 - Anticipation of Issues and Industry Groups

Materials for Volcanic Energy R&D in New Zealand/Japan (2000) , now Iceland (2012)

White Island, New Zealand: ?,000 MWe for ?? Years



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